IN THE SPECIFICATION:

Delete the paragraph beginning at page 3, line 33 and ending at page 3, line 34 of the present specification.

Insert the following paragraph immediately before the paragraph beginning on page 4, line 32 of the present specification:

> The effective temperature in the reactor is preferably between 400°C - 800°C. Further, the first combustion gas may be cooled to the effective temperature. Also, the sulphur content of the carbonaceous fuel is greater than 3% w/w, and the separated treated fuel preferably contains at least 8% w/w bound sulphur. In a further preferred embodiment, the carbonaceous fuel is selected from the group consisting of coal and petroleum coke containing at least 5% w/w sulphur.

Amend the paragraph beginning at page 5, line 16 and ending at page 5, line 20 of the present specification as follows:

> In order that the invention may be better understood, preferred embodiments will now be described, by way of example only, with reference to the drawing wherein the figure ~~Figure 1~~ is a diagrammatic block flow diagram of an apparatus and process according to the invention.

Amend the paragraphs beginning at page 5, line 25, and ending at page 6, line 20 of the present specification as follows:

The figure ~~Fig. 1~~ shows generally as 10 a carbonaceous fuel-burning superheated steam generating apparatus and process having a steam generating combustion boiler 12, a steam generating reactor 14 and a gaseous pollutant scrubber 16.

Sulphur rich carbonaceous fuel (fluid coke 1 tonne; 6% w/w S) 18 is fed as stream 24 to boiler 12 and burnt in a 10% stoichiometric excess oxygen atmosphere 20, fed as stream 22, to produce a first combustion oxygen-lean gaseous stream ~~22~~ 50 at 760°C containing

78.3 Kmol CO_2,
1.875 Kmol SO_2, in
8.02 Kmol O_2 and 332.0 Kmol N_2,

2.25×10^{10} J heat is recovered which generates 2.06×10^3 KWh electricity, on a 33% thermal energy conversion factor.

Reactor 14 receives gaseous stream ~~22~~ 50 and additional fluid coke (6% w/w S, 94% C) feed [[24]] 25, wherein the oxygen in stream 22 is used up by coke [[24]] 25 to form additional CO_2 and wherein the SO_2 is reduced by the coke 25 to elemental sulphur 26 and treated coke 28. These reactions are exothermic and produce ~~3.67 x 10^9KJ~~ 8.3×10^9 J of high grade heat which generates ~~??~~ 0.75×10^3 KWh electricity.

In alternative embodiments, additional oxygen (air) and/or SO_2 (not shown) additional to that contained in stream 22 may be injected into reactor 14.

Thus, the coke 25 introduced into reactor 14 serves initially to remove residual oxygen, but then reduces the SO_2 to produce elemental sulphur, CO_2 and treated coke, or activated carbon ~~30~~ 28.

Exhaust gas 32 as a ~~second~~ combustion gaseous stream exiting reactor 14~~,~~ Is cooled to provide superheated steam for electricity generation, to a temperature of about 200ºC and subsequently cooled further to about 120°C to condense the elemental sulphur for removal as product 26.

Exhaust gas 32, now with elemental sulphur removed, is passed to a scrubber ~~34~~ 16 containing all or a portion of treated coke ~~30~~ 28, which generally contains at least 10% w/w S and absorbs any SOx contaminants to provide an environmentally acceptable off-gas 36 and contaminated coke 38.